

Flow Instabilities & Turbulence in Viscoelastic Fluids

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Inertial instabilities in Newtonian
cross-slot flow - A comparison
against the viscoelastic bifurcation



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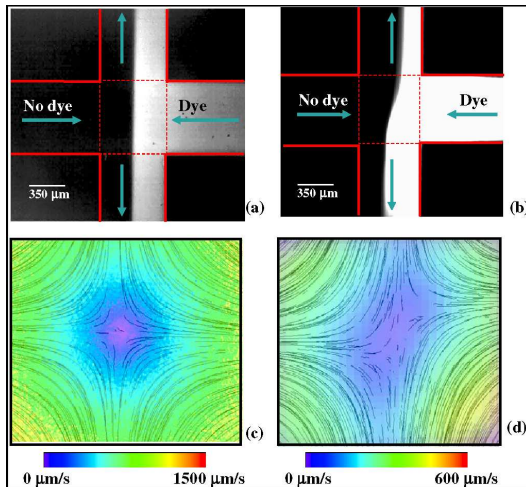
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Viscoelastic Flow

(inertia is neglected, $Re \approx 0$)

Arratia et al., *Phys. Rev. Lett.* **96**, 144502 (2006)

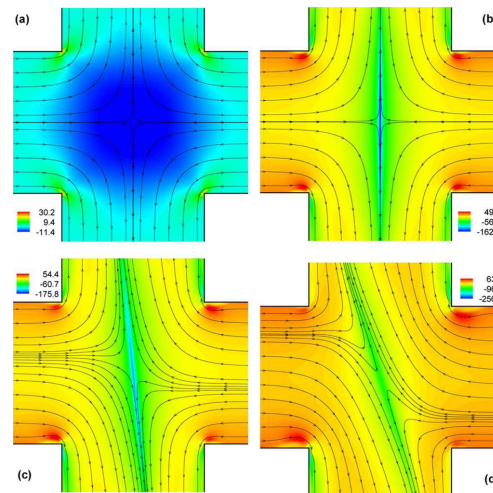
Results: Experimental



Newtonian $Re < 10^{-2}$ PAA solution $De = 4.5; Re < 10^{-2}$

Poole et al., *Phys. Rev. Lett.* **99**, 164503 (2007)

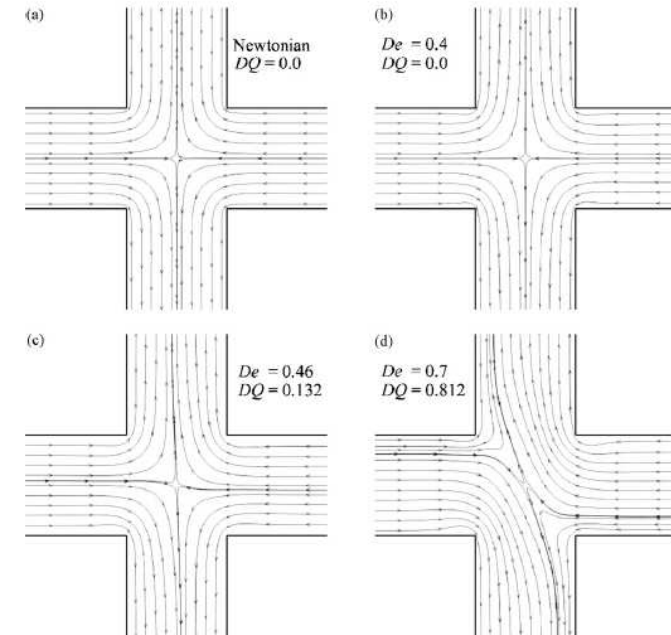
Numerical: UCM model



Contours of $N_1 (\tau_{xx} - \tau_{yy})$ with streamlines superimposed for:
(a) Newtonian fluid, (b) $De = 0.3$,
(c) $De = 0.32$ e (d) $De = 0.4$

Rocha et al., *J. Non-Newt. Fluid Mech.* **156**, 58-69 (2009)

Numerical: FENE-CR & FENE-P



Streamlines for: (a) newtonian fluid, (b) $De = 0.40$, (c) $De = 0.46$ e (d) $De = 0.70$
(FENE-CR, $L^2 = 100$ and $\beta = 0.1$)



Objective

- Investigate inertial effects in 2D Newtonian flow through a cross-slot
- Will a supercritical pitchfork bifurcation occur?
- Contrast the resulting instability with that for viscoelastic flow at $Re=0$



Equations

Assume 2D laminar, steady and incompressible flow

(1) **Mass conservation:**
$$\frac{\partial u_i}{\partial x_i} = 0$$

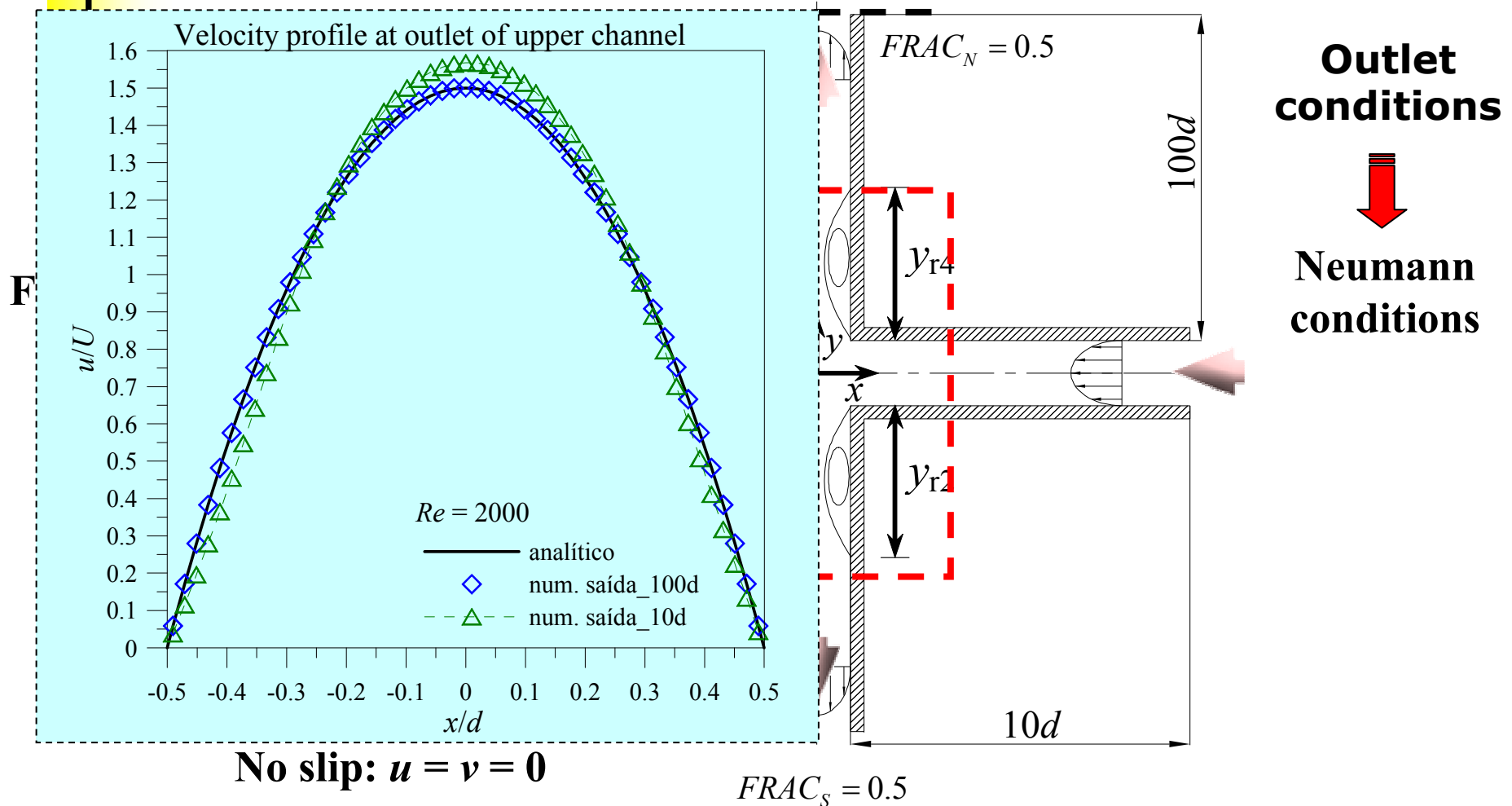
(2) **Momentum conservation:**

$$\rho \left(\frac{\partial u_i}{\partial t} + u_j \frac{\partial u_i}{\partial x_j} \right) = - \frac{\partial p}{\partial x_i} + \frac{\partial \tau_{ij}}{\partial x_j}$$

(3) **Constitutive Eq. (Newton law of viscosity):**

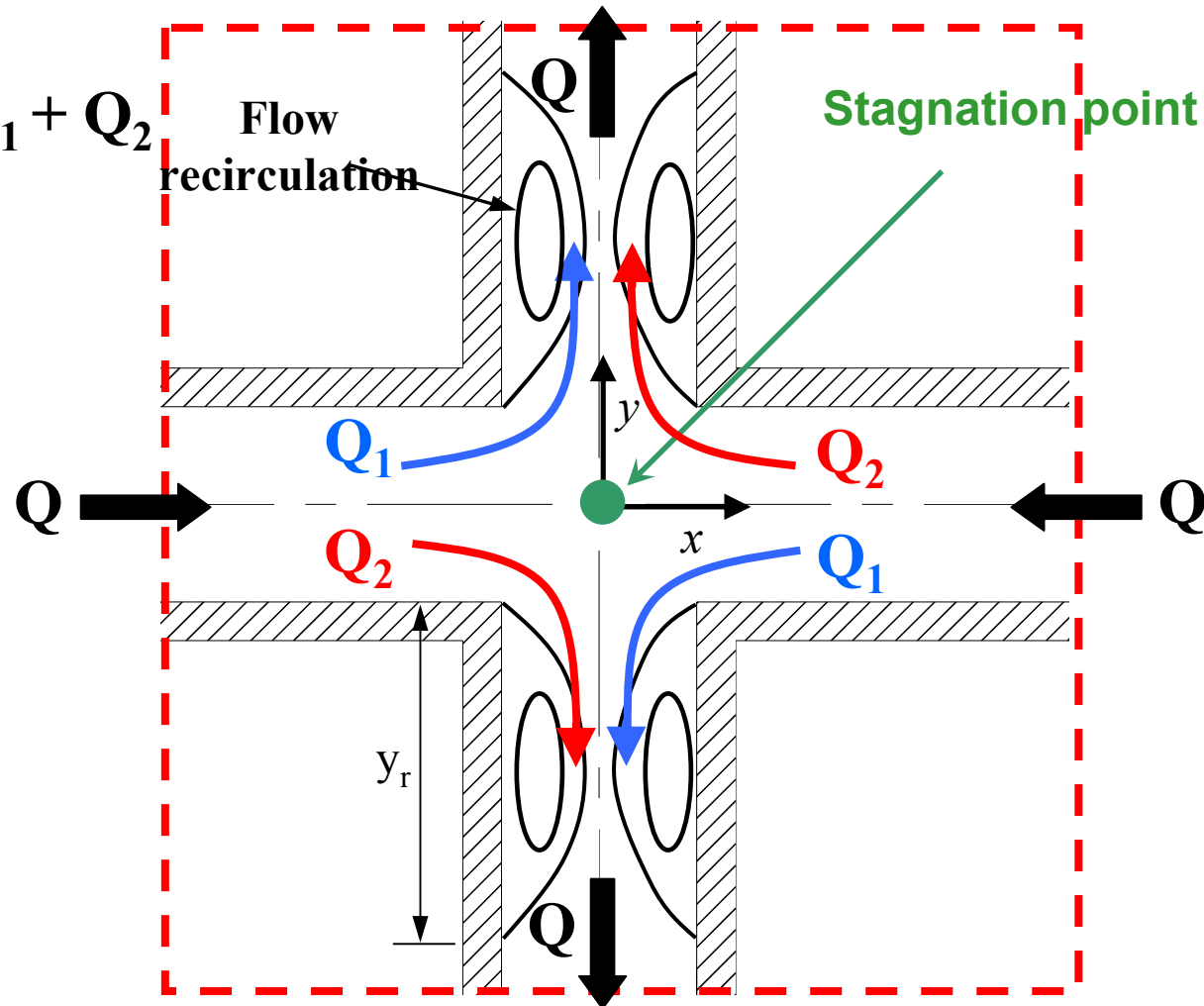
$$\tau_{ij} = \mu \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$

Geometry and boundary conditions



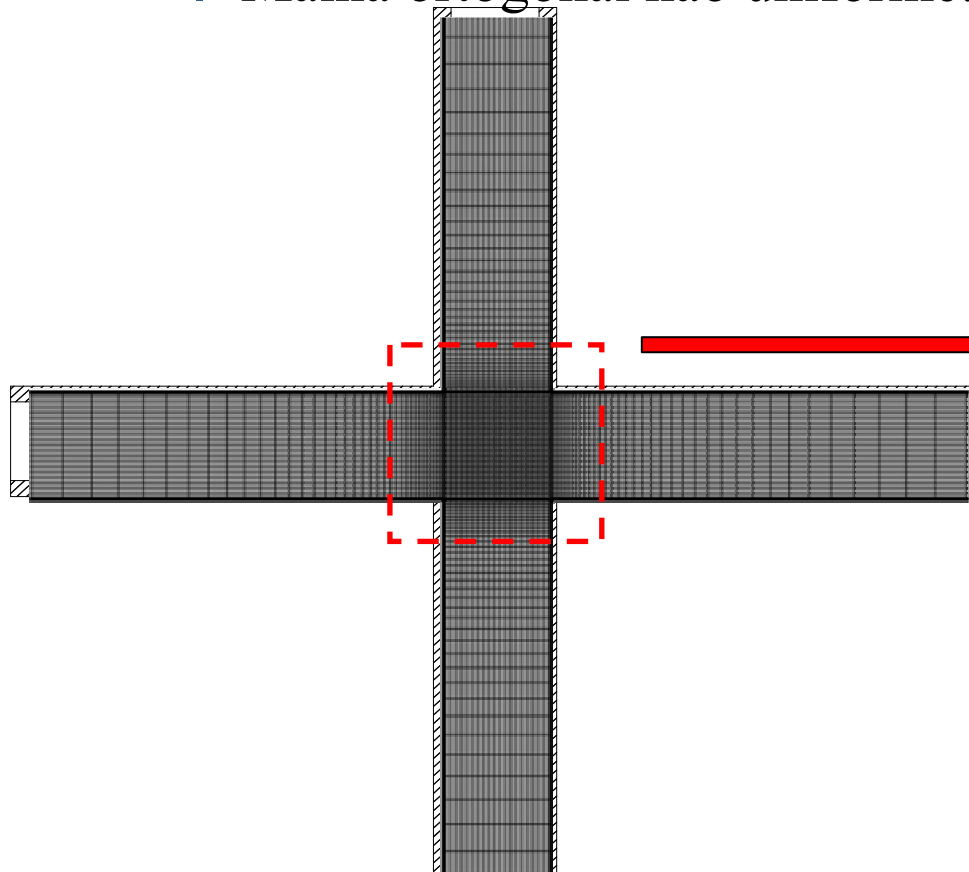
Geometry and boundary conditions

$$Q = Ud = Q_1 + Q_2$$



Numerical method

- Finite volume method (Oliveira *et al.*, JNNFM (1998)):
 - Equations discretized over a mesh;
 - Malha ortogonal não uniforme: $\Delta x_{\min} = \Delta y_{\min} \approx 0.02d$



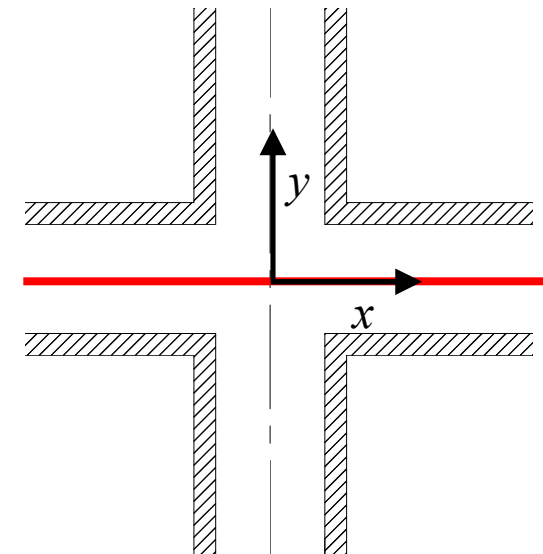
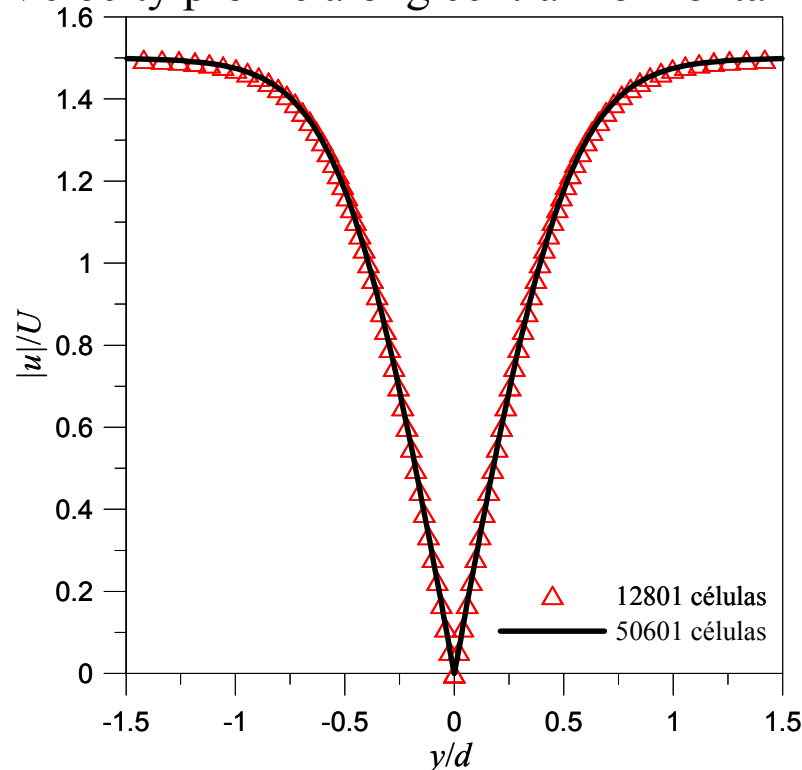
Blocos	M	f_v
I		1.000000
II		1.000000
III		0.929296
IV		1.075369
V		1.000000
NVC = 12801		

Mesh refinement

Controlling
parameter:

$$Re = \frac{\rho U d}{\mu}$$

Velocity profile along central horizontal line ($y = 0$) at $Re = 1400$.



Volumes controlo

Tamanho mínimo células

Malha 1

12801

$$\Delta x_{\min} = \Delta y_{\min} \approx 0.02d$$

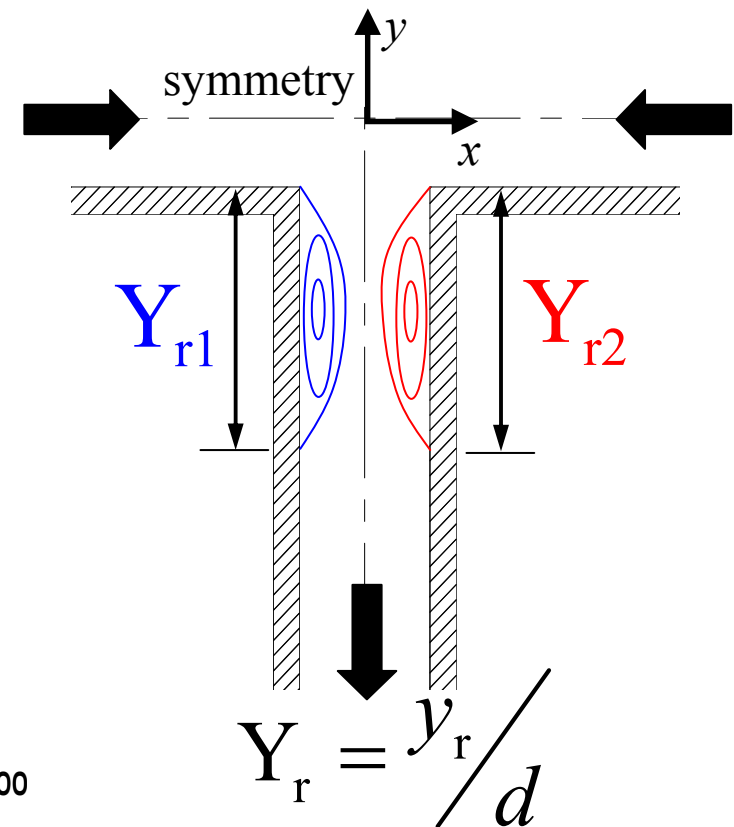
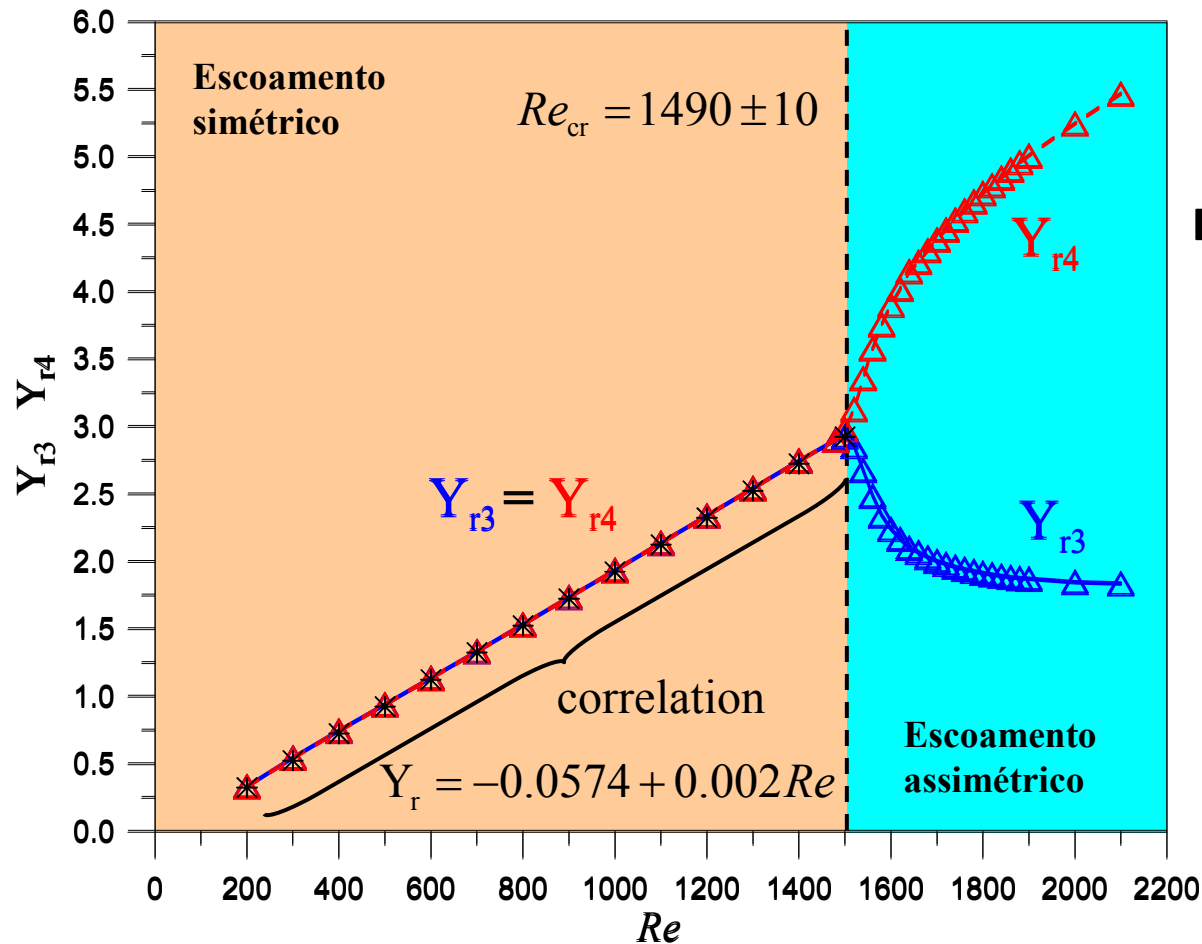
Malha 2

50601

$$\Delta x_{\min} = \Delta y_{\min} \approx 0.01d$$

Results

Influence of inertia (Re) upon the size of the two eddies on the lower outlet channel

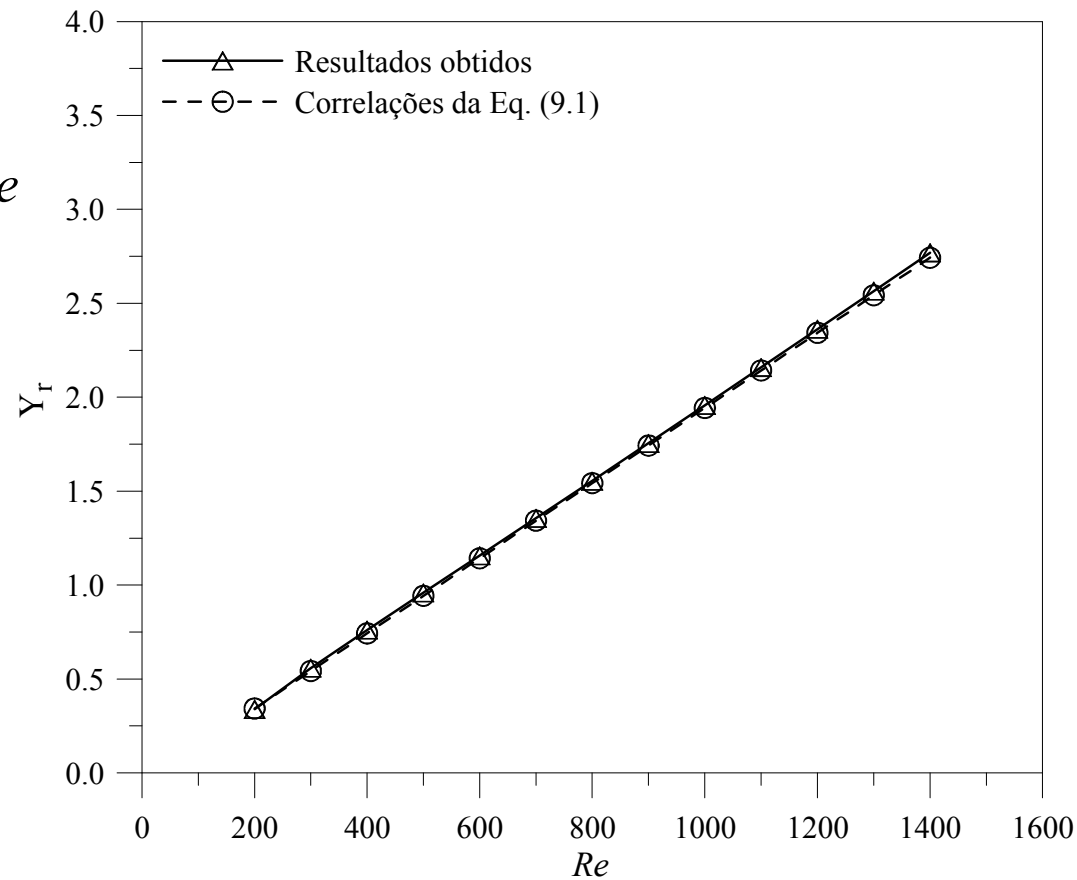


Results: correlation for eddy size

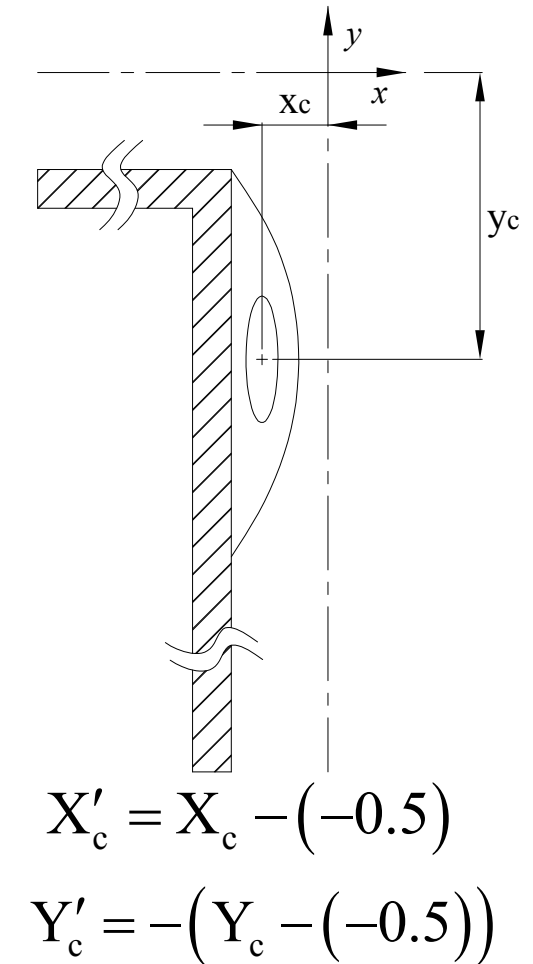
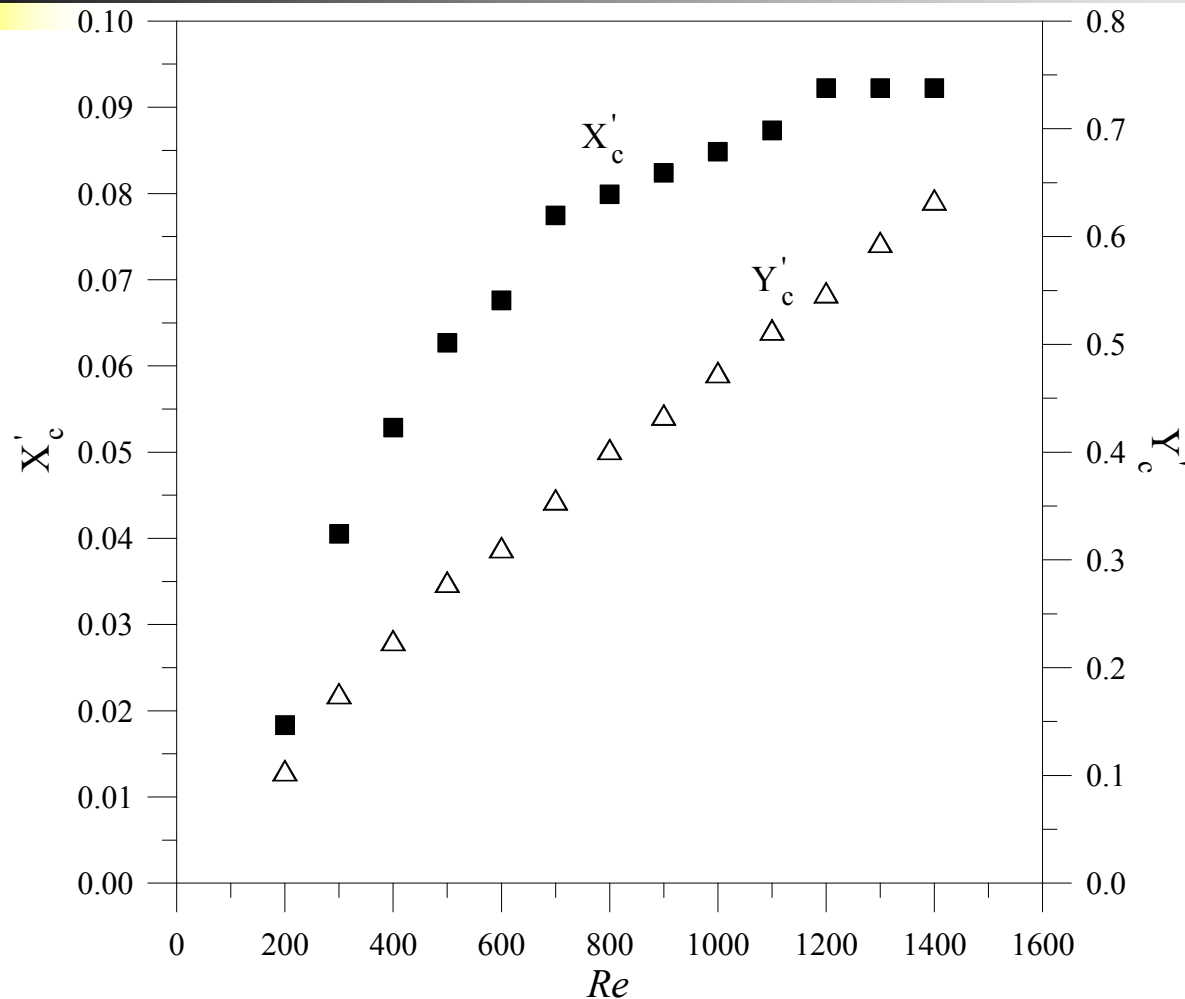
Correlation:

$$Y_r = -0.0574 + 0.002Re$$

$$200 \leq Re \leq 1500$$

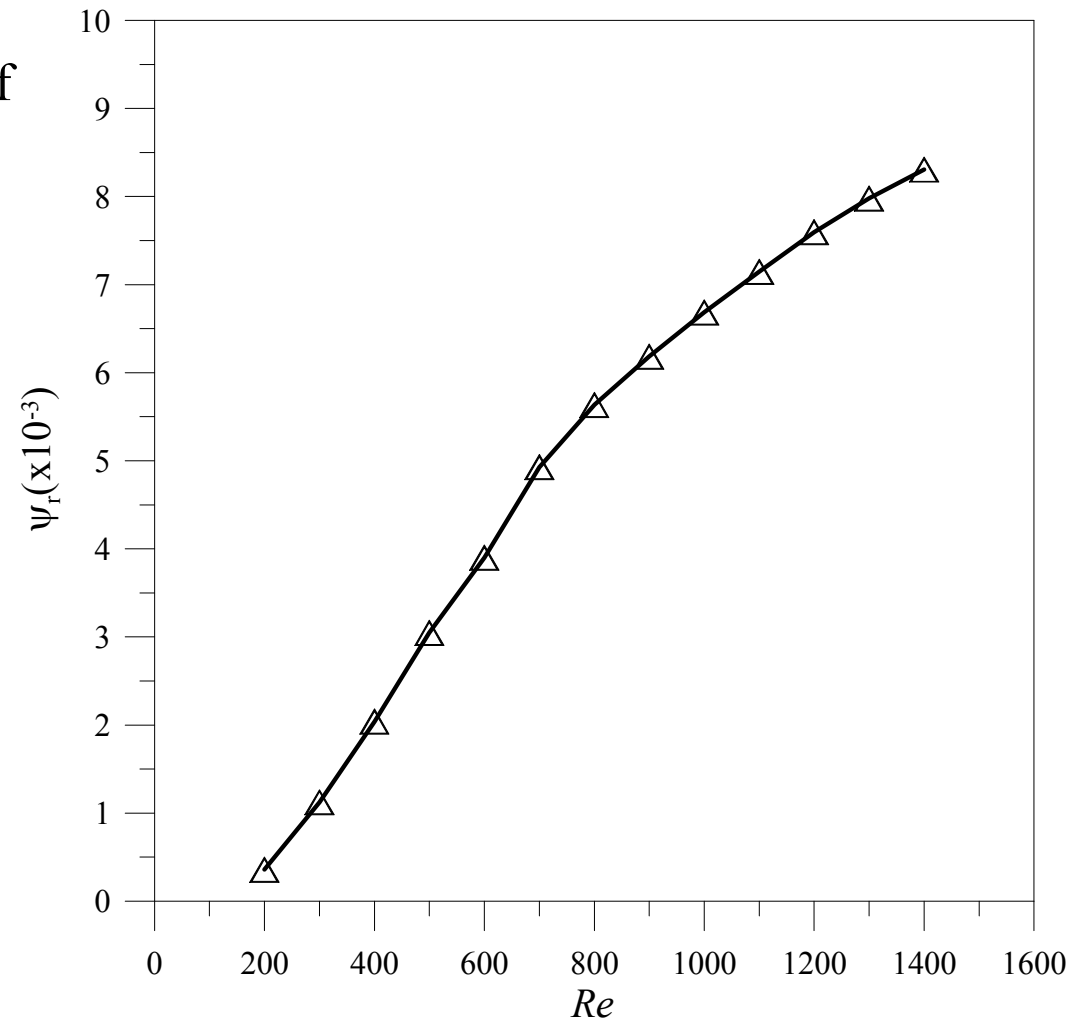


Results: eddy centre position (sym. flow)



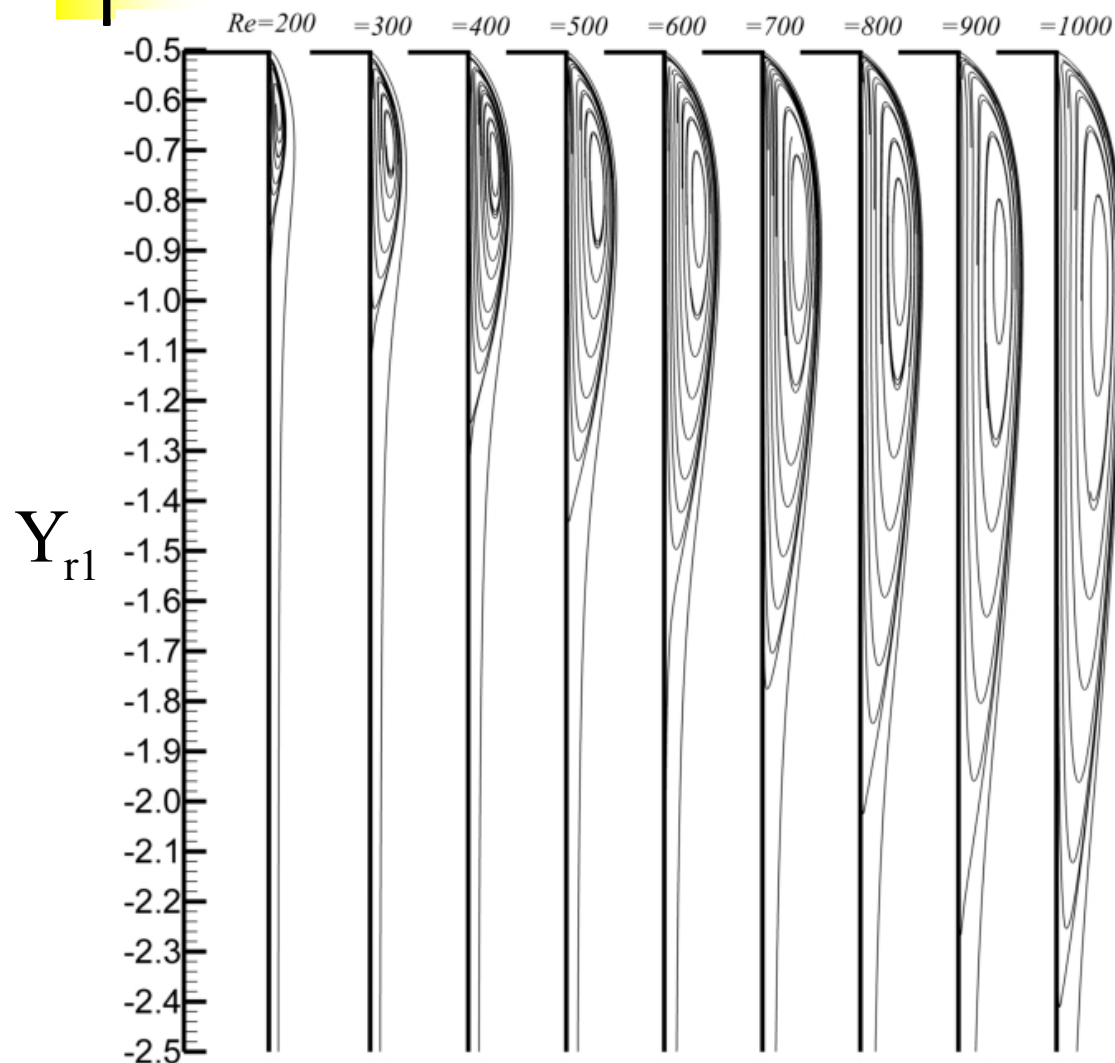
Results: eddy strength (symmetric flow)

Intensity as a function of
Reynolds number:

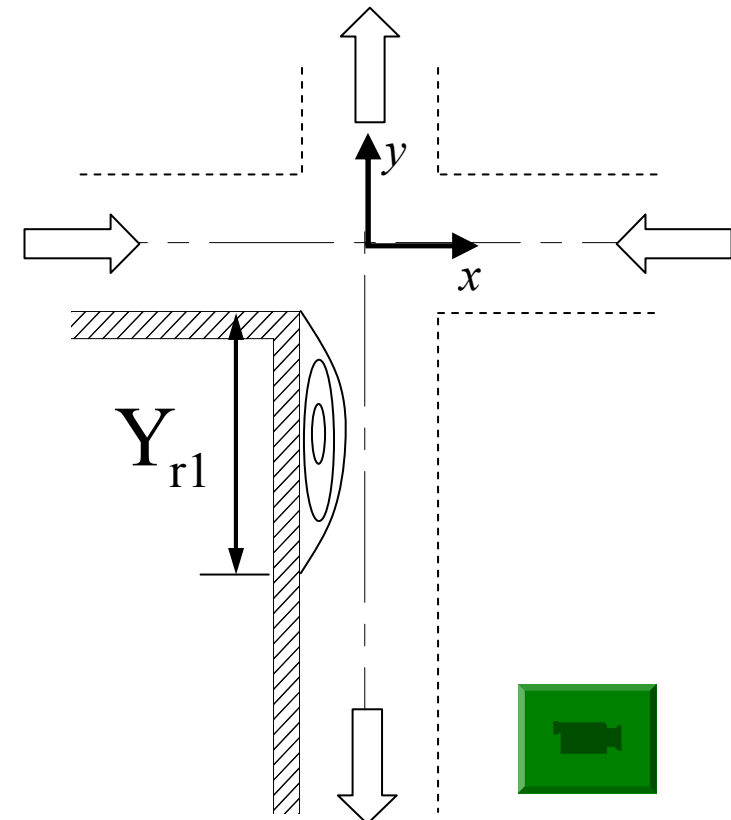


$$200 \leq Re \leq 1400$$

Results: streamlines (symmetric flow)



Detail of the eddy attached to the left wall of the lower outlet channel for increasing values of Reynolds number



Results: bifurcation parameter

To quantify the degree of asymmetry:

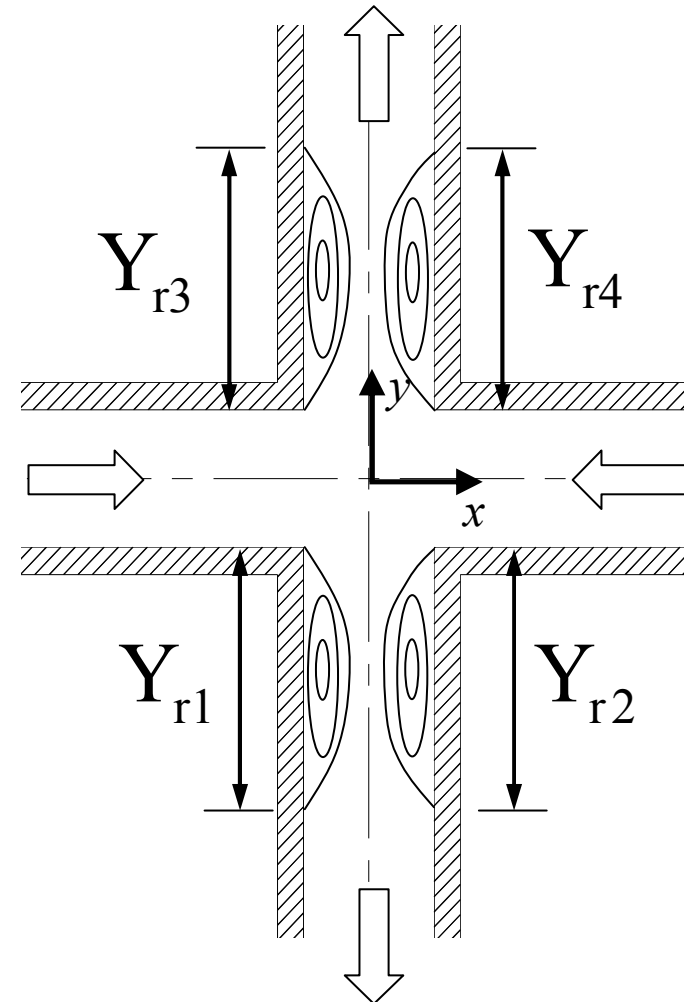
$$DY = -\frac{Y_{r2} - Y_{r1}}{\frac{1}{2}(Y_{r2} + Y_{r1})} = \frac{Y_{r4} - Y_{r3}}{\frac{1}{2}(Y_{r4} + Y_{r3})}$$

For symmetric flow:

$$Y_{r1} = Y_{r2} = Y_{r3} = Y_{r4} \Rightarrow DY = 0$$

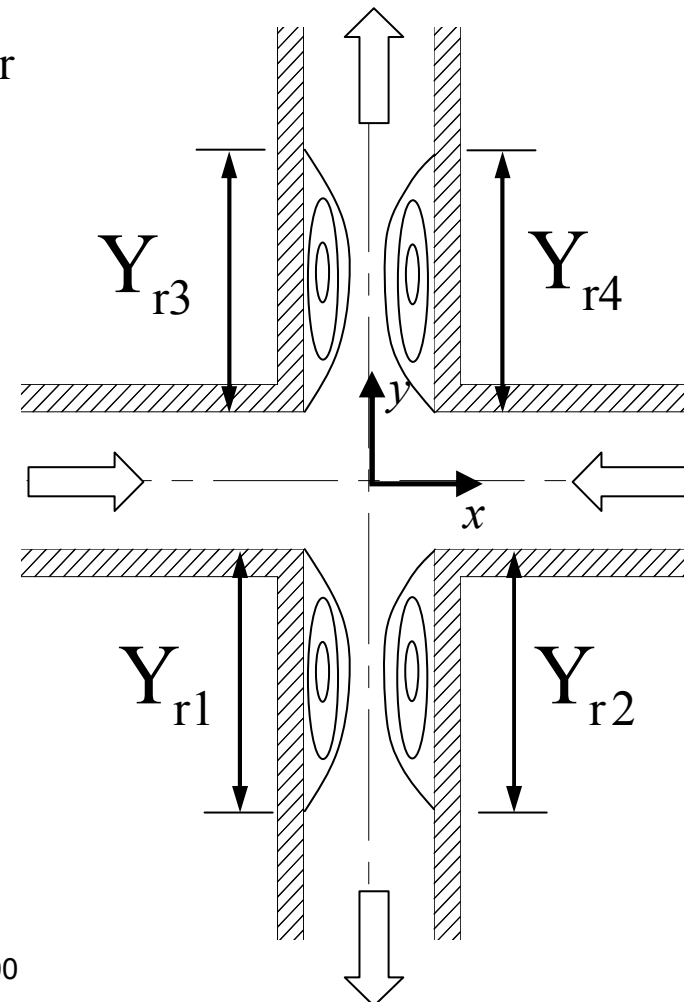
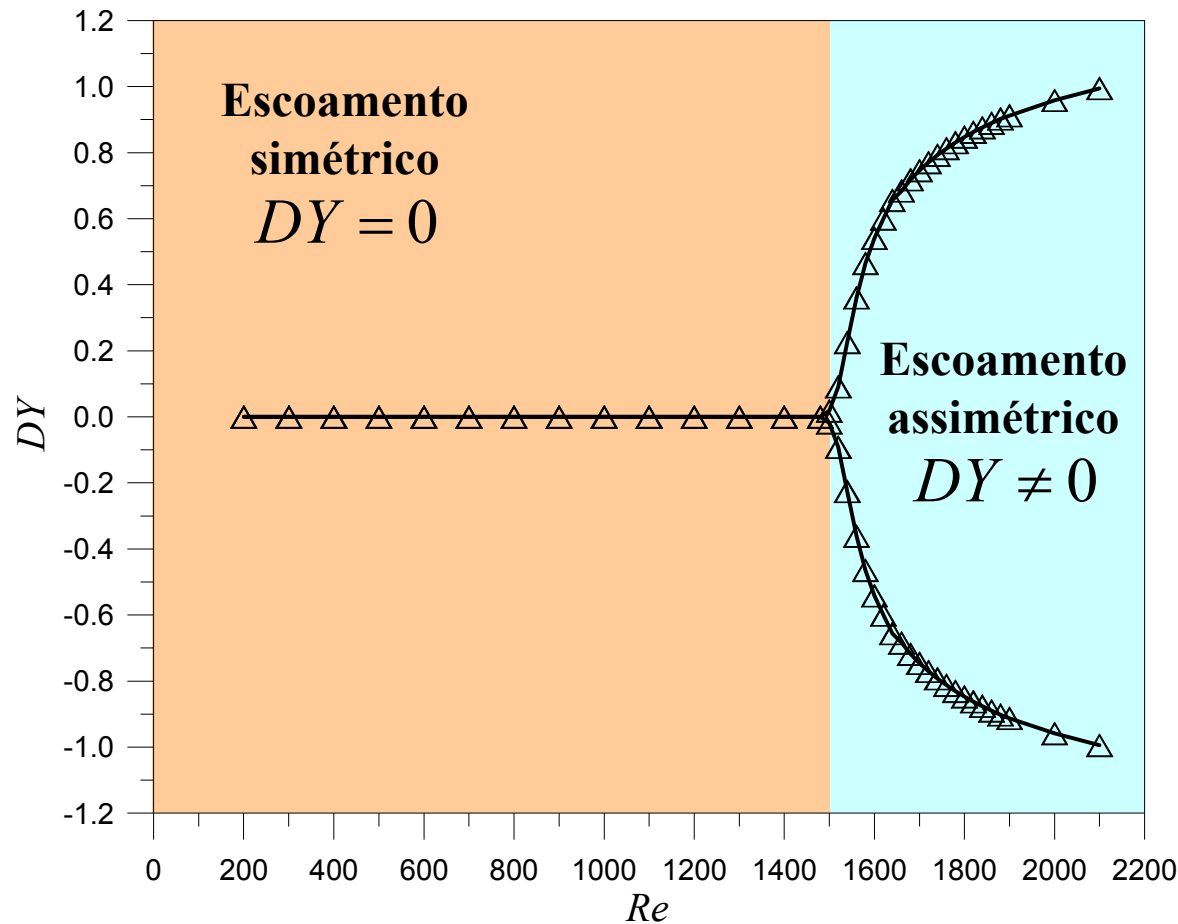
For asymmetric flow:

$$Y_{r1} = Y_{r3} \text{ e } Y_{r2} = Y_{r4} \Rightarrow DY \neq 0$$

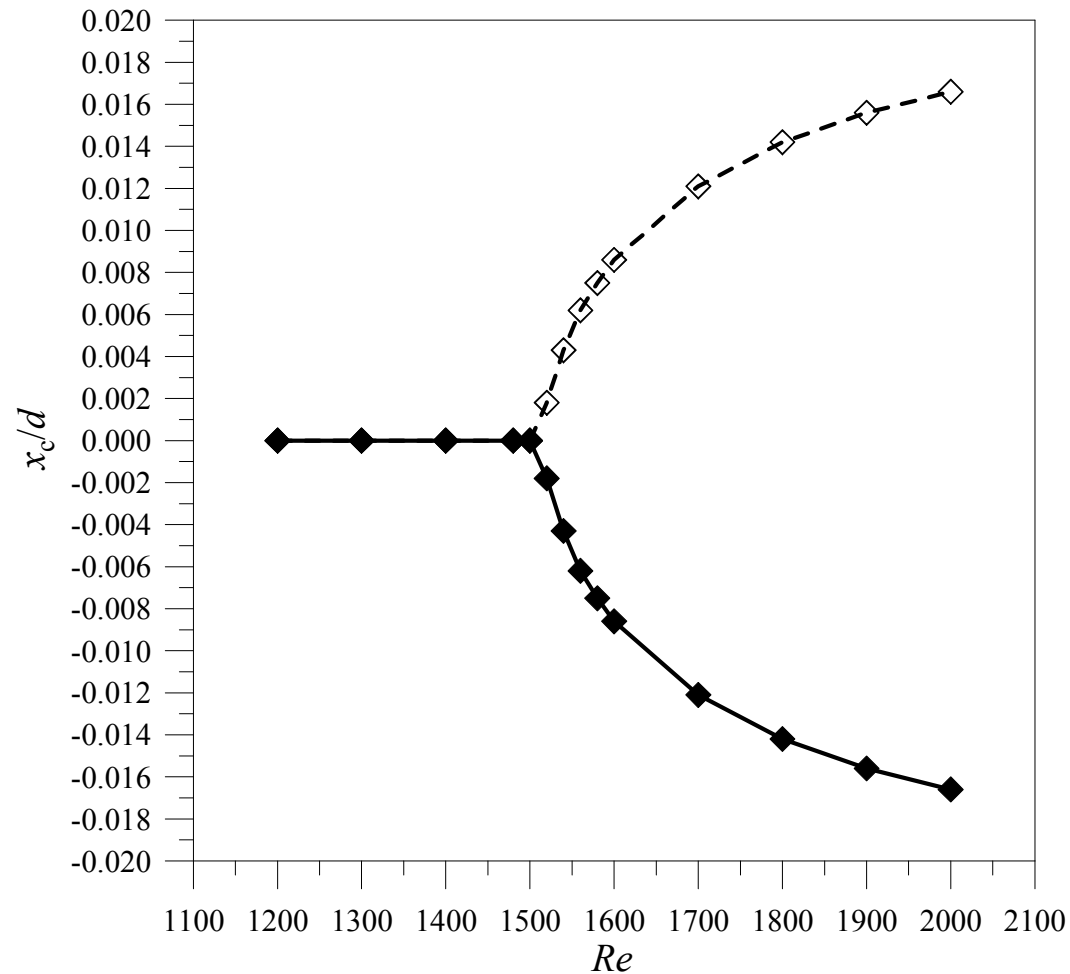


Results: bifurcation diagram

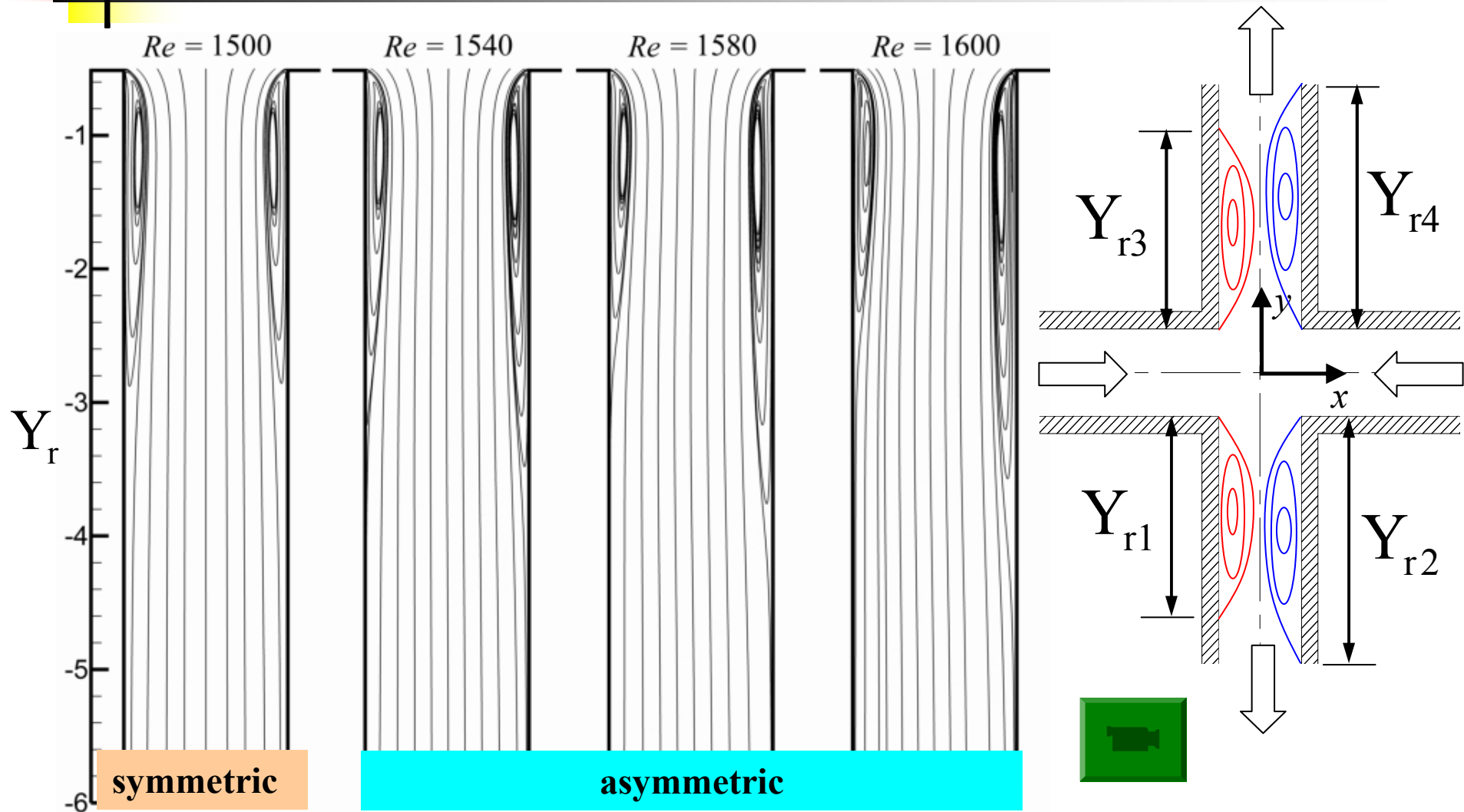
Bifurcation diagram: DY as a function of Reynolds number



Results: stagnation point position



Results: streamlines (asymmetric flow)



Results: pressure variation (1)

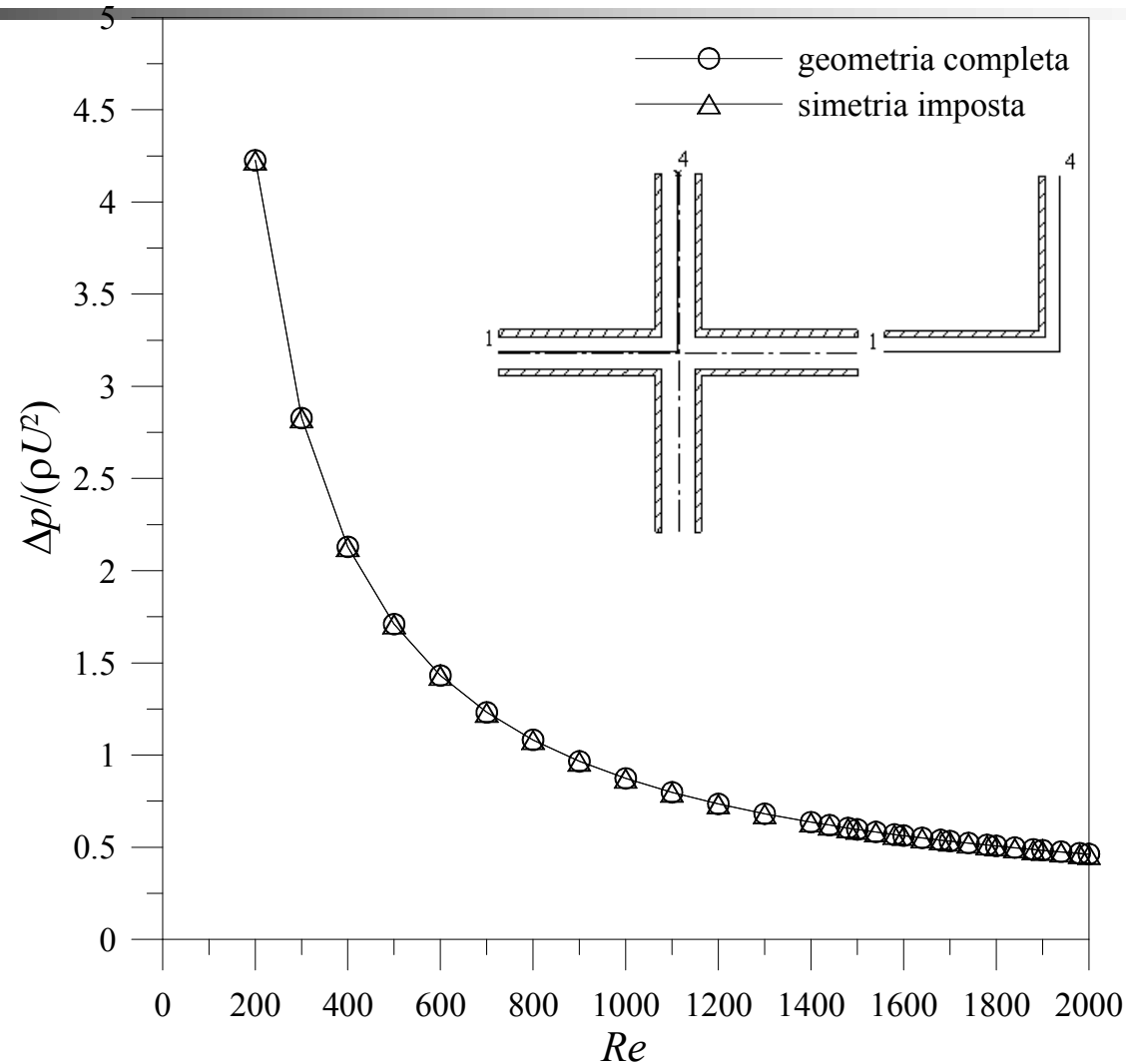
Compare full
geometry against
quarter of geometry
(full symmetry
imposed)

$$\Delta p = p_1 - p_4$$

Note: large part is

$$\frac{\Delta p_{FD} / \rho U^2}{L/d} = f$$

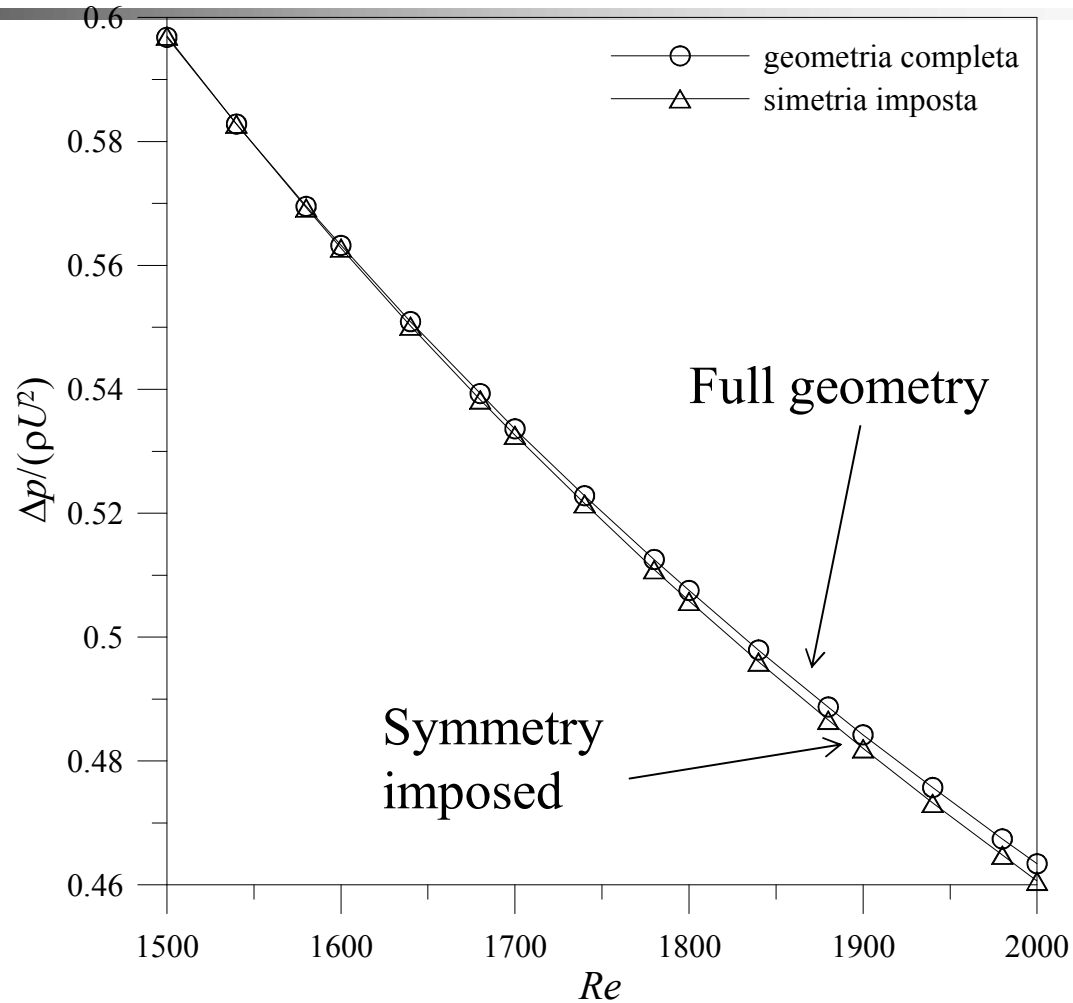
$$f = 12/Re$$



Results: pressure variation (2)

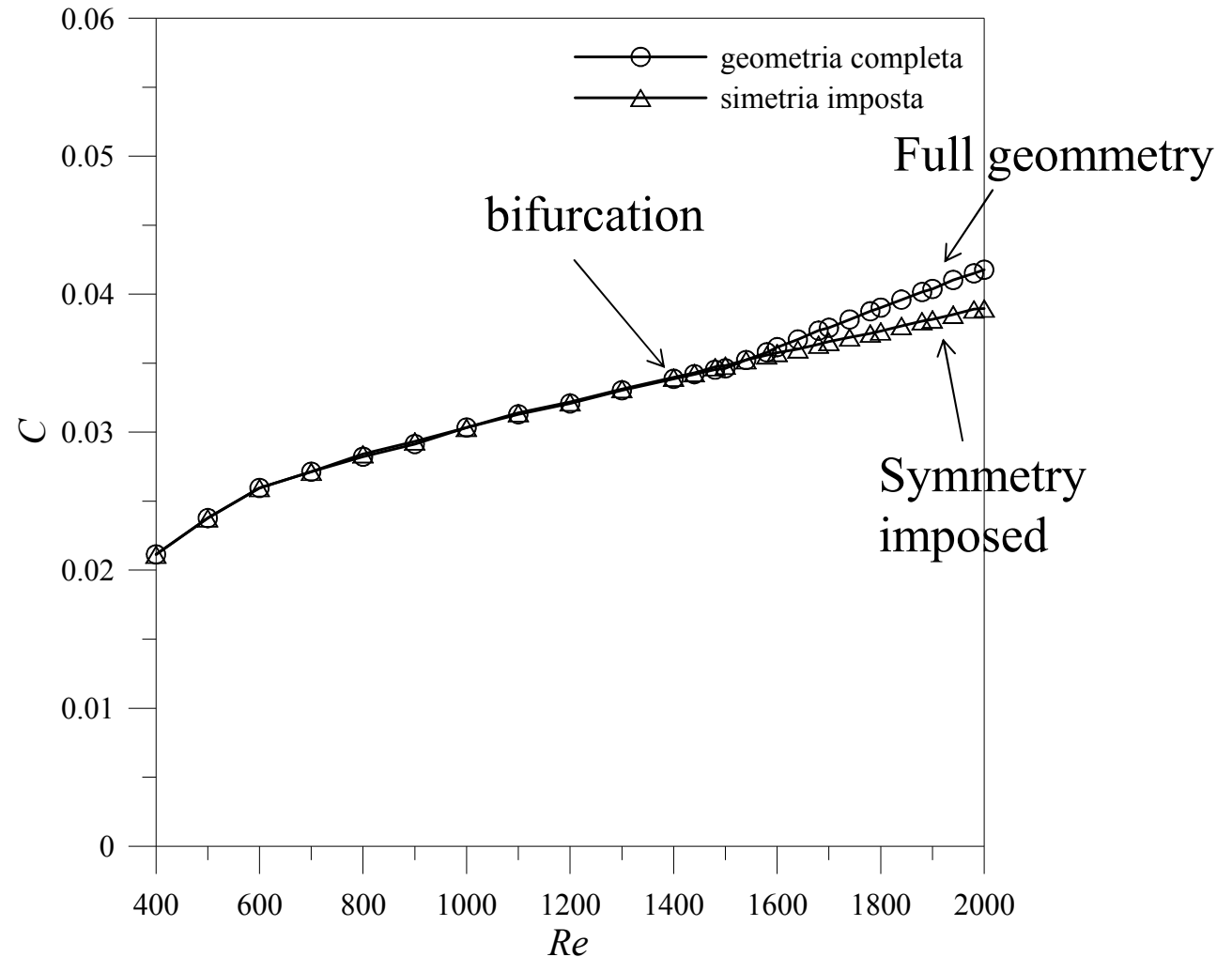
Detail for
 $1500 < Re < 2000$

$$\Delta p_{asym} > \Delta p_{sym}$$



Results: Couette correction

$$C = (\Delta p - \Delta p_{FD}) / \rho U^2$$



Conclusions

- ✚ **Inertia** provokes the appearance ($Re > 190$) of attached eddies, after the corners on the walls of outlet channels.
- ✚ The **size of those eddies** increases linearly with Re , while the flow remains symmetric (up to $Re_{cr} = 1490 \pm 10$).
- ✚ When $Re > Re_{cr}$ the flow becomes **asymmetric**, with larger eddies on one side of the walls, as compared to the opposite wall.
- ✚ The size of the smaller eddies tend to remain constant with Re , while the larger eddies keep increasing in size.
- ✚ The **symmetry** of the flow pattern after bifurcation is different from the viscoelastic case at low Re .



Acknowledgments

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